



# Article Magnetron Sputtered Low-Platinum Loading Electrode as HER Catalyst for PEM Electrolysis

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**Abstract:** The development of cost-effective components for Proton Exchange Membrane (PEM) electrolyzers plays a crucial role in the transformation of renewable energy into hydrogen. To achieve this goal, two main issues should be addressed: reducing the Platinum Group Metal (PGM) content present on the electrodes and finding a large-scale electrode manufacturing method. Magnetron sputtering could solve these hurdles since it allows the production of highly pure thin films in a single-step process and is a well-established industrial and automated technique for thin film deposition. In this work, we have developed an ultra-low 0.1 mg cm<sup>-2</sup> Pt loading electrode using magnetron sputtering gas aggregation method (MSGA), directly depositing the Pt nanoparticles on top of the carbon substrate, followed by a complete evaluation of the electrochemical properties of the sputtered electrolyzer cell. They demonstrate similar efficiency to commercial electrodes with a Pt content of 0.3 mg/cm<sup>2</sup>, achieving a 67% reduction in Pt loading. Additionally, durability tests indicate that these electrodes offer greater stability compared to their commercial counterparts. Thus, magnetron sputtering has been proven as a promising technology for manufacturing optimum high-performance electrodes at an industrial scale.

Keywords: magnetron sputtering; hydrogen evolution reaction; low Pt loading

### 1. Introduction

As the concern about climate change and the urgency to mitigate its devastating consequences are increasing rapidly, it is crucial to radically change our fuel-based energy system towards a more sustainable approach based on renewable energy sources that allow complete decarbonization of the energy sector. In recent years, hydrogen has arisen as the ideal energy carrier, mainly due to its high energy density per molecule; the only byproduct of  $H_2$  combustion is water, and it can be obtained directly by water electrolysis [1–4]. There are several types of electrolysis using renewable energy sources, and among these, one of the most relevant is the proton membrane exchange (PEM) electrolysis [5–8]. This is due to several factors like low-temperature operation, achievement of high current densities at low voltages, negligible membrane gas crossover, and compact system design [9]. Despite these advantages, the main issue with PEM electrolysis is the high price of its components, especially the catalysts. In the anode, for the OER (oxygen evolution reaction), the most effective catalysts are Ir or  $IrO_x$ , whereas in the cathode, for the HER (hydrogen evolution reaction) is Pt, both being highly scarce and expensive elements. Currently, for PEM electrolyzers with a catalyst-coated membrane configuration (CCM), the Pt loadings in the cathode are high, around 3 to 1 mg cm<sup>-2</sup> [10,11]. In principle, decreasing the Pt loading could be achieved without compromising the electrolyzer's efficiency. This is



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**Copyright:** © 2024 by the authors. Licensee MDPI, Basel, Switzerland. This article is an open access article distributed under the terms and conditions of the Creative Commons Attribution (CC BY) license (https:// creativecommons.org/licenses/by/ 4.0/). because the exceptionally fast kinetics of Pt for the HER allow the use of low Pt loadings, hence significantly reducing the production costs of the stack [12–14]. Currently, catalytic coatings are developed using wet chemical methods like wet chemical impregnation, solgel, or thermal decomposition. For instance, Pt nanoparticles synthesized through these methods are often mixed with an ionomer and high-surface carbon black powder to avoid nanoparticle agglomeration. The obtained catalytic ink usually has to be deposited by spraying techniques over the membrane or the gas diffusion layer (GDL) [2,15,16]. Wet chemistry methods provide a high surface area to the catalytic layer, which is crucial to obtaining a high catalytic surface. However, these techniques have multiple drawbacks, such as reaction byproducts and multiple reaction steps, which are directly related to material waste and complex industrial upscaling.

Magnetron sputtering appears to be a compelling manufacturing method for solving these issues. As a robust industrial single-step process for thin film deposition, magnetron sputtering not only reduces the waste of material with the absence of byproducts but also facilitates the upscaling of catalysts manufacturing for large-scale production of electrodes for PEM electrolyzers. As far as we know, the use of magnetron sputtering as a manufacturing method for platinum group metals (PGMs) PEM electrolysis catalysts is not very wide, especially for the cathode side [17–19]. Most of the existing research work is focused on the ex-situ evaluation of the HER catalyst, where the a huge potential of magnetron sputtering for their application [12,20–24]. To the best of our knowledge, a couple of research works have been published regarding in-situ single-cell testing. For example, Pt thin films were deposited over titanium multifunctional liquid/gas diffusion layers in order to evaluate HER activity and H<sub>2</sub> bubbles behavior inside a PEM single-cell [25]. This research work proved that most of the catalysis seems to occur on the surface of the electrode. In another study, a stirring cup for the carbon powder was introduced inside a magnetron-sputtering laboratory chamber, and Pt nanoparticles were deposited over the carbon support using a direct current (DC) power source [26]. Several loadings of Pt were evaluated for PEM electrolysis and fuel cell, showing no performance differences with electrodes developed using chemical methods. Hence, if HER catalysis is a process that occurs only on the electrode surface with no catalytic activity differences from the traditional synthesized catalyst, magnetron sputtering could be a feasible alternative to industrially upscale PEM catalyst.

As far as we are concerned, there is a complete lack of research on the use of magnetron sputtering to develop Pt nanoparticles for PEMWE and critically reduce the presence of Pt in the cathode. In this work, we have developed an ultra-low 0.1 mg cm<sup>-2</sup> Pt loading electrode using magnetron sputtering, directly depositing the Pt nanoparticles on top of a carbon microporous layer (MPL) GDL, followed by a complete evaluation of the electrochemical properties of the sputtered electrode. This method enables a full exposure of Pt nanoparticles to the reactants, maintaining a high surface area while reducing the Pt loading. The aim of this research is to prove the feasibility of magnetron sputtering as an electrode manufacturing technique, allowing Pt reduction without interfering with cell performance. The electrochemical evaluation was performed in a three-electrode cell and a single PEM cell, and the results were compared with a commercial 0.3 mg cm<sup>-2</sup> Pt/C electrode for both electrochemical setups. Electrochemical ex-situ analysis techniques like cyclic voltammetry and linear sweep voltammetry (CV, LSV) were measured for all samples to evaluate the catalytic activity for HER in an acidic electrolyte and in-situ analysis through V-i curves and chronopotentiometry measurements (CP), was performed in a real single PEM cell to evaluate the performance and degradation of both electrodes.

#### 2. Materials and Methods

### 2.1. Platinum Nanoparticles Deposition

Pt nanoparticles were deposited over a microporous layer of carbon paper (Sigracet 22BB MPL, with 5% polytetrafluoroethylene (PTFE)) with a coated surface of 1 cm<sup>2</sup> for the ex-situ and 25 cm<sup>2</sup> for the in-situ tests. The gas aggregation system (NanoGenTrio, Mantis Deposition Ltd., Thame, UK) was attached to an industrial PVD chamber ( $80 \times 60 \text{ cm}^2$ ),

coupled with a 4 mm hole, enabling particles to move from one chamber to the other. The platinum target ( $2.54 \times 3 \text{ cm}^2$ , purity of 99.999%) was positioned on a mobile sputter head, with a distance of 9.5 cm from the chamber hole. The base pressure of the whole vacuum system was  $2 \times 10^{-4}$  Pa, and the target was cleaned before starting the deposition process for 2 min at 15 W with a 4 Pa Ar pressure. After a previous process optimization [12], an Ar flux of 30 sccm and He flux of 15 sccm, corresponding to a total pressure of 14 Pa, were introduced in the aggregation chamber. To start the sputtering process to obtain the Pt nanoparticles, a discharge power of 25 W was applied for 15 min. The sputtered electrodes were compared with a commercial 0.3 mg cm<sup>-2</sup> Pt electrode (40%wt Pt/C, Sigracet 22BB MPL, with 5% PTFE. The MSGA method is the most suitable magnetron sputtering technique for nanoparticle deposition. In contrast with traditional magnetron sputtering, in MSGA, the sputtering takes place inside a high-pressure aggregation chamber where supersaturated vapors of the ejected material enable the formation of clusters or nanoparticles of well-defined size and shape. As the sputtered particles collide with inert gas atoms, their energy is lowered and begins to condense into small clusters. These clusters serve as nuclei, where additional particles coalesce, leading to the formation of larger nanoparticles [27–31].

## 2.2. Characterization Methods

The size and morphology of the nanoparticles Pt electrodes were studied using a ULTRA Plus Carl-Zeiss (Jena, Germany) field emission scanning electron microscope (FESEM) and a TECNAI G2 20 TWIN (Hillsboro, OR, USA) high-resolution transmission electron microscope at an acceleration voltage of 200 kV (STEM). A SPECS customized system with a nonmonochromatic X-ray source XR 50 and a hemispherical energy analyzer PHOIBOS 150 (SPECS Surface Nano Analysis GmbH, Berlin, Germany) was used to assess the relative abundance of the surface species. Thermogravimetric analysis (TGA) was performed using a TA Instruments Q500 instrument (New Castle, DE, USA) equipped with an EGA furnace to determine the Pt loading of the experimental and commercial samples. The measurements were conducted from r. t. until 900 °C using a 10 °C min<sup>-1</sup> heating ramp in air flow (90 mL min<sup>-1</sup>).

## 2.3. Electrochemical Characterization

For the ex-situ test in a three-electrode cell, an Autolab PGstat 302 N (Tokyo, Japan) potentiostat was used to perform cyclic voltammetry (CV) and linear sweep voltammetry (LSV) measurements recorded with Nova software (https://www.metrohm.com/es\_es/service/software-center/nova.html). The three-electrode cell setup had an Ag/AgCl (3 M KCl) electrode and a Pt wire as reference and counter electrodes, respectively. The working electrodes were the sputtered and commercial electrodes with an exposed area of 1 cm<sup>2</sup>. CV measurements for Pt surface cleaning and activation were recorded between 0.05 and 1.23 V at 50 mV s<sup>-1</sup> until a constant signal was obtained. The data was collected in 0.5 M H<sub>2</sub>SO<sub>4</sub> electrolyte at room temperature in an Ar atmosphere. LSV measurements were recorded between 0.01 and -0.3 V at 5 mV s<sup>-1</sup> in an Ar-saturated 0.5 M H<sub>2</sub>SO<sub>4</sub> electrolyte for HER evaluation. To determine the *iR* drop [32], the solution resistance (Rs) was obtained by electrochemical impedance spectroscopy (EIS) at a frequency interval of 0.1 Hz–100 kHz with a 10 mV perturbation. The overpotential (η) at a current density of 10 mA cm<sup>-2</sup> and the Tafel slopes obtained in the corresponding cathodic overpotential range were extracted from the corrected *iR* polarization curves in order to benchmark catalysts' activity.

A PEM test bench from H2GREEM was used for in-situ characterization in a single cell designed in Tekniker (Figure 1). The MEA was composed of commercial catalyst-coated Nafion 115 membranes (127  $\mu$ m of thickness) only coated with 3 mg cm<sup>-2</sup> loading of IrRuO<sub>x</sub> on the anode side (Fuel Cell Store, Bryan, TX, USA, EE.UU.). For the cathode, a commercial GDL with 0.3 mg cm<sup>-2</sup> Pt electrode (40%wt Pt/C, Sigracet 22BB MPL, with 5% PTFE, from Fuel Cell Store) was established as the reference and with the same MPL-GDL. Also, a 0.1 mg cm<sup>-2</sup> Pt sputtered electrode was measured. Both anode and cathode were

equipped with an ultrathin platinized titanium (grade 2) porous transport layer (PTL) with a nominal thickness of 250  $\mu$ m, a 30% porosity, and 5–10  $\mu$ m of pore diameter (Fuel Cell Store, EE.UU.). As flow channels, two PEEK frames and two titanium meshes of 1 mm were used to distribute and evacuate the water and formed gases. To stabilize the cell and activate the catalysts, a current density of 0.12 A cm<sup>-2</sup> was applied for 24 h. Measurements were performed at 60 °C with a deionized H<sub>2</sub>O flow rate of 0.2 L min<sup>-1</sup>. Polarization curves were measured every 24 h for a week, ranging from 0.12 to 2 A cm<sup>-2</sup>. Between these measurements, the cell was maintained at a current density of 1.5 A cm<sup>-2</sup> to assess the stability of the two Pt GDLs.



Figure 1. Scheme of the PEM single-cell components.

## 3. Results and Discussion

# 3.1. Characterization

XPS measurements were performed to determine the chemical composition and oxidation state of the Pt nanoparticles on the sputtered electrode (Figure S1), confirming the presence of only metallic Pt species, thus the purity of the coatings. For the observation and comparison of the surface morphology of the sputtered and commercial electrodes, images of the surface were obtained by SEM (Figure 2). The sputtered Pt electrode (PtS\_GDE) clearly shows a rough surface formed by nanoparticles (Figure 2a), while the commercial sample (PtCom\_GDE) presented a smoother surface as Pt nanoparticles are mixed with the carbon black powder (Figure 2b). In the sputtered sample, all of the Pt nanoparticles are on the electrode surface, potentially increasing Pt exposure to the electrolyte.

The size and nanoparticle distribution of the electrodes were analyzed using TEM images. The diameter of 100 nanoparticles was measured from the images to elaborate the PtS\_GDE nanoparticle size statistic size histogram. An average size of around 4 nm was obtained with a narrow size distribution from 2 to 6 nm (Figure 3b) for the PtS\_GDE sample, and most parts of the Pt nanoparticles showed a well-defined spherical shape (Figure 3a). High-angle annular dark-field scanning TEM (HAADF-STEM) images reveal that Pt nanoparticles on the PtCom\_GDE sample are scattered inside the carbon black powder (Figure 3d), while Pt nanoparticles on PtS\_GDE are deposited only on the surface of the carbon black MPL. In the case of the PtS\_GDE, as a consequence of the high surface area of the MPL, the thickness is non-homogeneous (Figure 3c).

Finally, the Pt content of both samples was obtained from thermogravimetric analyses. The initial weight loss (approximately 17% between 500 and 590 °C) is related to the presence of PTFE in the carbonaceous substrate. In the range of 590–750 °C (around 81%), the rest of the carbon species are calcinated, and the remaining mass corresponds to Pt, the only compound that is stable at high temperatures. Hence, Pt loading was obtained from the mass at the highest analysis temperature. Two measurements were performed for each electrode, and the results show that PtCom\_GDE has a Pt loading of  $3.93 \pm 1.58$  wt% (0.3 mg cm<sup>-2</sup>) while PtS\_GDE contains  $1.37 \pm 0.29\%$  (0.105 mg cm<sup>-2</sup>) (Figure 3e). This is a remarkable reduction in the Pt loading of 67% with respect to the 0.3 mg cm<sup>-2</sup> Pt/C commercial electrode.



Figure 2. SEM images of (a) PtS\_GDE and (b) PtCom\_GDE.

## 3.2. Electrochemical Characterization

The cyclic voltammogram of the sputtered sample after stabilization in the Ar-saturated 0.5 M  $H_2SO_4$  electrolyte is depicted in Figure 4. The observed peaks correspond with the reported for polycrystalline Pt with an  $H_{upd}$  region between 0.05 and 0.4 V, followed by the double layer region and, towards more positive potentials, the Pt-oxide formation region. Moving to more negative potential values, the reduction of Pt oxides can be observed in the reserves scan around ca. 0.8 V [33].



**Figure 3.** STEM images of (**a**) PtS\_GDE, (**b**) size distribution histogram and cross-section colored HAAF-STEM images of (**c**) PtS\_GDE and (**d**) PtCom\_GDE and (**e**) TGA measurements of PtS\_GDE.



Figure 4. Cyclic voltammetry of PtS\_GDE.

To evaluate and compare the HER activity of both electrodes, a potential sweep from 0 V vs. RHE towards cathodic potential values was recorded in the Ar atmosphere. Figure 5 shows the polarization curves where the overpotentials needed to reach a current density value of  $-10 \text{ mA cm}^2$  are the reference for the evaluation of the HER activity of different catalysts [34,35]. As presented in Figure 6, the overpotential for a current density of  $-10 \text{ mA cm}^2$  of the PtCom\_GDE sample is 74 mV, while the overpotential at the same current density for the PtS\_GDE is 53 mV. These results are preliminary proof that Pt loading can be reduced without compromising the electrode activity towards the HER. Besides, the reduction of the overpotential, when compared to the commercial sample, could be influenced by the fact that in the sputtered electrode, all Pt nanoparticles are placed on the surface in direct contact with the reactant, while in the commercial sample, the Pt active sites can be more difficult to reach since they are mixed with the MPL powder.



Figure 5. LSV curves of PtS\_GDE and PtCom\_GDE in an Ar-saturated 0.5 M H<sub>2</sub>SO<sub>4</sub> solution.

Regarding the kinetic parameters of both electrodes, the Tafel slope for the HER reaction was extracted from the Tafel curves shown in Figure 6. At an acidic pH, the HER occurs through two reaction pathways: Volmer Heyrovsky or Volmer-Tafel. For

polycrystalline Pt, the reported values are over 30–40 mV dec<sup>-1</sup>, which corresponds to the Volmer-Tafel pathway [36,37]. Tafel slopes for PtS\_GDE and PtCom\_GDE are 32.8 and 58.8 mV dec<sup>-1</sup>, respectively, which are in concordance with the reported values for polycrystalline Pt. In the case of the PtCom\_GDE, the slope is slightly higher than for PtS\_GDE, meaning that the HER is happening at a slower pace in the case of the commercial sample. As Pt nanoparticles are mixed with the carbon MPL, this could hinder the access of the reactants to the active sites and the release of gas bubbles, slowing the reaction rate [25].



Figure 6. Tafel plots of PtS\_GDE and PtCom\_GDE.

Since the results of the ex-situ tests indicated that the Pt sputtering electrodes performed better than the commercial ones, in situ tests in electrolysis cells were conducted. Measurements were carried out as described in Section 2.3 in a self-designed single cell. After the 24 h preconditioning, polarization *V-i* curves were performed every 24 h, applying stationary current densities of 1.5 A cm<sup>-2</sup> between each curve. Figure 7 shows the recorded *V-i* curves at 0 h, 24 h, 72 h, and 168 h for PtCom\_GDE (Figure 7a) and PtS\_GDE (Figure 7b).

When using the PtCom\_GDE sample as the cathode, t = 0 h curve, the potential corresponding to a current density of 1 A cm<sup>-2</sup> is 1.85 V. This potential value increases up to 1.93 V after 168 h of operation. For the PtS\_GDE, the initial t = 0 h *V-i* curve shows slightly higher voltages at the second half of the current density sweep compared to the rest of the polarization curves. Nevertheless, the voltage stabilizes completely after the first polarization curve. Figure 8 compares the *V-i* curves at 0 h and 168 h for both samples, demonstrating that, under the same conditions, the PtS\_GDE electrode is more stable with time than the PtCom\_GDE sample. Both start with 1.85 V at 1 A cm<sup>-2</sup>; however, at t = 168 h, the potential value is maintained nearly the same for the PtS\_GDE, whereas for the PtCom\_GDE electrode, the potential has increased over time.

This voltage variation is further observed in stationary current measurements. To estimate the degradation rate, operation potentials at stationary current densities were measured for 2 h every 20 h over a total period of 100 h. From the slope of the curve, the degradation rate can be extracted. Figure 9. presents the *V* vs. *t* graphic of PtCom\_GDE and PtS\_GDE. The same tendencies as seen in *V-i* curves are observed, hence proving the stability of the PtS\_GDE. The slope extracted from the linear regression of the PtCom\_GDE measurements corresponds to a degradation rate of 700  $\mu$ V h<sup>-1</sup> at an operation current density of 1.5 A cm<sup>-2</sup>. Meanwhile, the degradation rate for the PtS\_GDE is completely negligible, as the line is almost flat.



Figure 7. Polarization V-i curves at t 0 h, 24 h, 72 h, and 168 h of (a) PtCom\_GDE and (b) PtS\_GDE.

Summarizing all the results, it is evident that reducing the amount of Pt is not hindering the cell performance. In fact, using MSGA as a deposition method could enhance cell performance not only because all of the catalytic material is on the MPL surface but also because the deposited nanoparticles could be better attached to the surface as a consequence of an adhesion improvement. One of the major issues of Pt/C catalysts is the lack of adhesion and nanoparticle agglomeration, which negatively impacts performance [38,39].



Figure 8. Comparison of polarization V-i curves at t 0 h and 168 h of PtCom\_GDE and PtS\_GDE.



Figure 9. Comparison of voltage evolution with time of both samples.

#### 4. Conclusions

Pt-sputtered electrodes have been successfully developed by gas aggregation magnetron sputtering to study the effect of Pt loading reduction in the performance of a PEM single cell. The surface morphology and composition study confirmed that the catalytic surface was formed by spherical 4 nm pure Pt nanoparticles. The achievement of a 67% reduction in Pt compared with a 0.3 mg cm<sup>-2</sup> Pt/C commercial electrode without compromising cell performance content. Although the conditions used in this work need to be transferred and adapted to a magnetron sputtering process, this work proves that magnetron sputtering is a promising method to precisely reduce PGM loadings. Finally, from the obtained results, two main conclusions can be drawn:

- The amount of Pt is not directly related to an improvement in cell performance. The exposition of Pt active sites seems to be much more relevant than the Pt present in the catalytic coating.
- MSGA is confirmed as a practical and feasible manufacturing method for developing Pt HER electrodes. This technique successfully produces effective, stable, and effective electrodes in a step process, directly depositing pure Pt nanoparticles on the GDL.

Considering the obtained results, it can be confirmed that magnetron sputtering is a feasible manufacturing method for HER low Pt loading electrodes, enabling the reduction of Pt without worsening cell stability or affecting performance. Therefore, magnetron sputtering technology could be a promising technique for the large-scale production of competitive PEMWE electrodes.

**Supplementary Materials:** The following supporting information can be downloaded at: https://www.mdpi.com/article/10.3390/coatings14070868/s1, Figure S1. XPS Spectrum of the Pt 4f core-level region of PtS\_GDE Pt species.

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